



Economy Topic Team: *Hydrogen Station Costs*

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September 14, 2004

Introduction

- Motivation:
 - Put a price tag on the H2Hwy Network for different scenarios
 - Determine economical network configurations
- Questions:
 - How many stations?
 - What kind (e.g. electrolysis vs. reformation)?
 - How big (e.g. 10 vs. 100 kg/day?)
 - What are the benefits of Distributed Generation?
- Team Members
 - 30+ volunteers from public and private sector



$$\left[\frac{p^2}{2\mu} + V(r) \right] \psi(r) = E \psi(r)$$

Organization

1. Intro:

- purpose of talk, goals

2. Station Cost Model

- Methodology
- Stations Choices & Rationale
- Assumptions
- Model Validation

3. Results:

- Scenarios for Success
- Sensitivity Analysis

4. Energy Stations (covered by Tiax)

5. Conclusions



$$\left[\frac{p^2}{2\mu} + V(r) \right] \psi(r) = E \psi(r)$$

Methodology

GOAL 1: Obtain realistic near-term station costs

GOAL 2: Identify important factors that affect station cost

- Cost Validation
 - Data collected from industry for equipment, station construction, and operating costs
 - Scaled for size and expected 2010 production volume
 - Assumption Validation
 - Vetted with Economics Team, outside sources
 - Compared against assumptions in other reports
 - (e.g. NAS, Tiax, GM WTW)
 - Model Validation
 - Undergoing review within Team
- Forming Peer Review Committee



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Stations Analyzed

Type of Station	Design Capacity (kg H ₂ /day)	Average Fuel Demand (kg H ₂ /day)	Average Cars Refueled per day
Mobile Refueler	10	1	0.5
On-site Production (SMR and Electrolysis)	30, 100, 1000	3, 10, 100	1, 3, 33
Delivered Liquid Hydrogen	1,000	100	33
Average Gasoline Station	-	3,000 gal/day	375 conventional cars/day

Note: Assumes avg. H₂ demand of 0.66 kg/car/day (3 kg/fill) (based on 50 mpg, 12000 miles/yr), and 8 gallons gasoline per fill on average.

Capacity Factor = 10% (average consumption / rated production capacity).
For Liquid delivery and mobile station, rated capacity based on assumed daily fueling window.



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Design Assumptions (1)

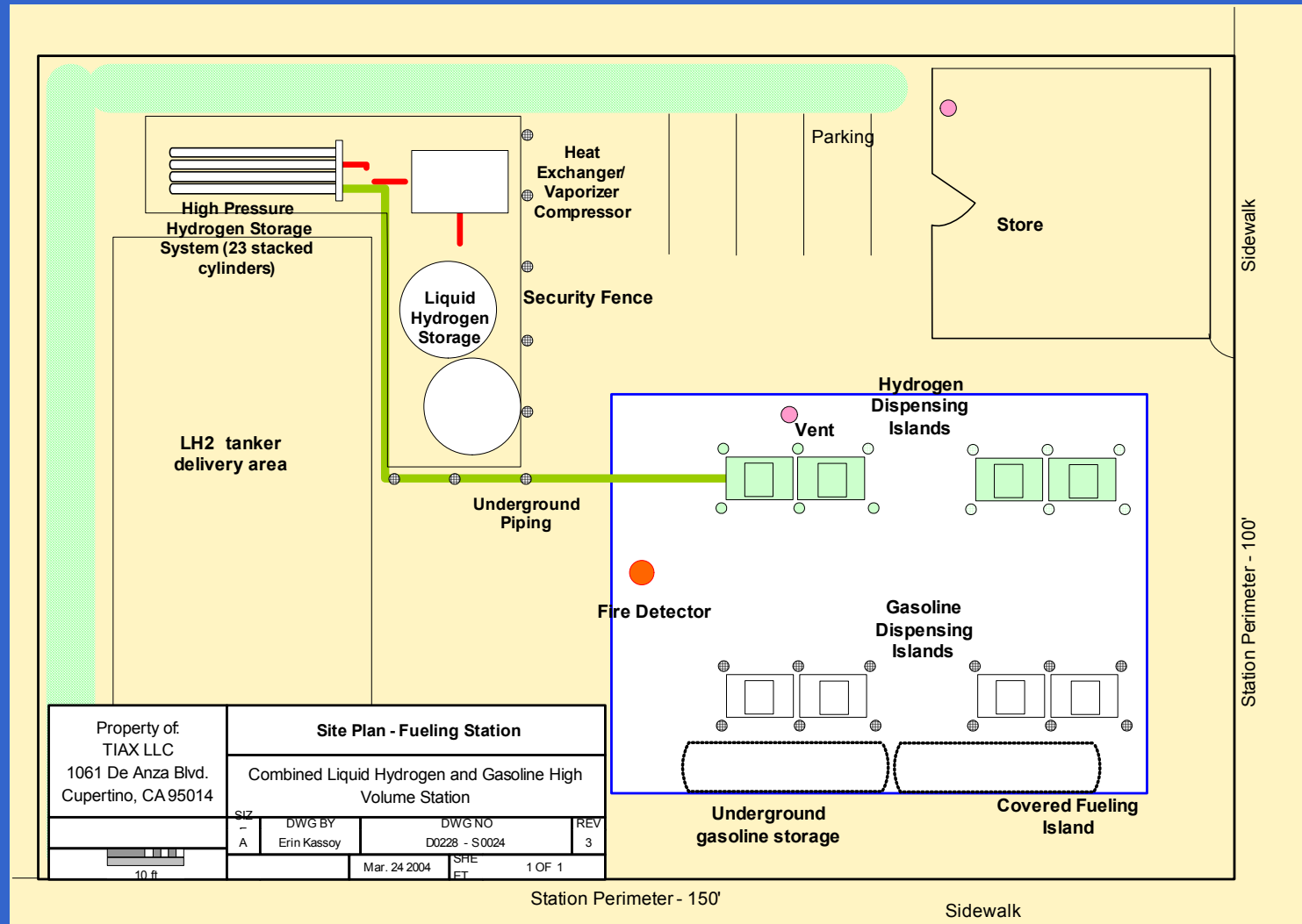
Station Type	Key Technology	Additional Components
Mobile Refueler	Integrated Refueler Trailer	Cascade storage/dispensing
Natural Gas Reformer	Steam Methane Reformer, Pressure Swing Absorption	Reciprocating-piston compressor, cascade storage/dispensing
Electrolyser	Alkaline Electrolyser	
Delivered LH ₂ Tanker Truck	Cryogenic Storage Tank, 6,250 Cryo-pump	evaporator + cascade storage dispensing

- Small and large H₂ stations are integrated into existing gasoline stations with 8 dispensers total
 - Small station = 1 cH₂ dispenser, Large station = 3 cH₂ dispensers



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Site Plan - LH2 Station Example



Note: Assumes 10% capacity factor and avg. H₂ demand of 0.65 kg/car/day (3-5 kg/fill) (based on 50 mpg, 12000 miles/yr), and 8 gallons gasoline per fill on average.

Design Assumptions (2)

- 6,250 psi dispensing compressed gaseous hydrogen
 - 5,000 psi on-board vehicle storage
- Storage and dispenser requirements based on rated station capacity
 - 2 daily peaks
 - 40% of total daily throughput in 3-hours



$$\left[\frac{p^2}{2\mu} + V(r) \right] \psi(r) = E \psi(r)$$

Economic Assumptions (1)

- Divide station operating labor between hydrogen / gasoline / non-fuel sales (1/8 or 3/8)
- Rent cost assumed for landscape and hardscape
 - Based on site plan
- Equipment costs based on industry costs and 2x today's production volumes
- Capital Cost amortized over 15 years with 10% return on investment
 - based on 15 year plant life
- Commercial utility rates



$$\left[\frac{P^2}{2\mu} + V(r) \right] \psi(r) = E \psi(r)$$

Economic Assumptions (2)

- Energy Prices based on review of several projections/forecasts (ISE Research)
 - Electricity
 - 9.7 cents/kWh California Energy Commission
 - 12.4 cents/kWh Chevron Texaco
 - 4 cents/kWh City of San Francisco, 12.4 cents/kWh
 - Natural Gas
 - 6.68 \$/MMBtu Depart of Energy EIA
 - 5.93 \$/MMBtu Wall Street Journal



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Model Validation

- Assumptions compared to existing hydrogen reports:
 - Authur D. Little, GM, SFA Pacific, National Academy of Science
- Verifying assumptions with industry (e.g. electrolysis efficiency) revealed some reports too optimistic.

Parameter	Study	On-site NG Reformation	Electrolysis
Total Electric Consumption (kWh/kg)	<i>H2Hwy 2010</i>	3.0	60
	Lasher/ADL	3.41	53.45
	GM/LBST	2.16	53.84
	Simbeck/SFA Pacific	2.19	54.8
Natural Gas Consumption (J/J)	<i>H2Hwy 2010</i>	1.35	-
	Lasher/ADL	1.32	-
	Simbeck/SFA Pacific	1.43	-

H2Hwy Network Assumptions

– 10% station capacity factor, 5000 vehicles served

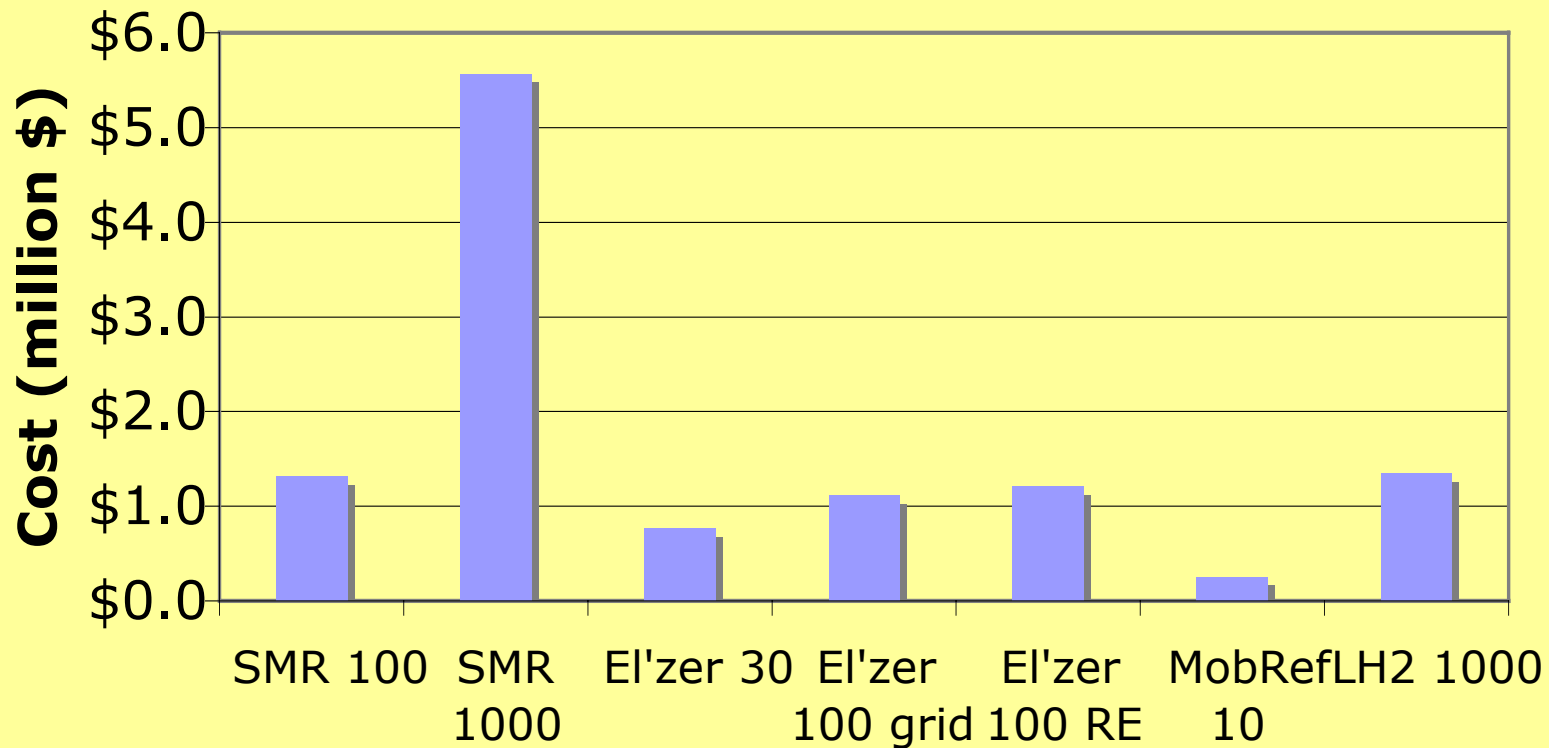
Station Type	%	# of Stations	Cost (MM\$/ Station)
1. Steam Methane Reformer, 100	8%	19	\$1.32
2. Steam Methane Reformer, 1000	4%	10	\$5.57
3. Electrolyzer, grid 30	15%	36	\$0.76
4. Electrolyzer, grid 100	4%	10	\$1.11
5. Electrolyzer, renewable energy 100	15%	36	\$1.21
6. Mobile Refueler 10	38%	92	\$0.25
7. Delivered LH2 1000	5%	12	\$1.34
8. Energy Stations and Specialty Stations	11%	27	\$1.58
Total	100%	242	

H2Hwy Cost: Baseline Scenario

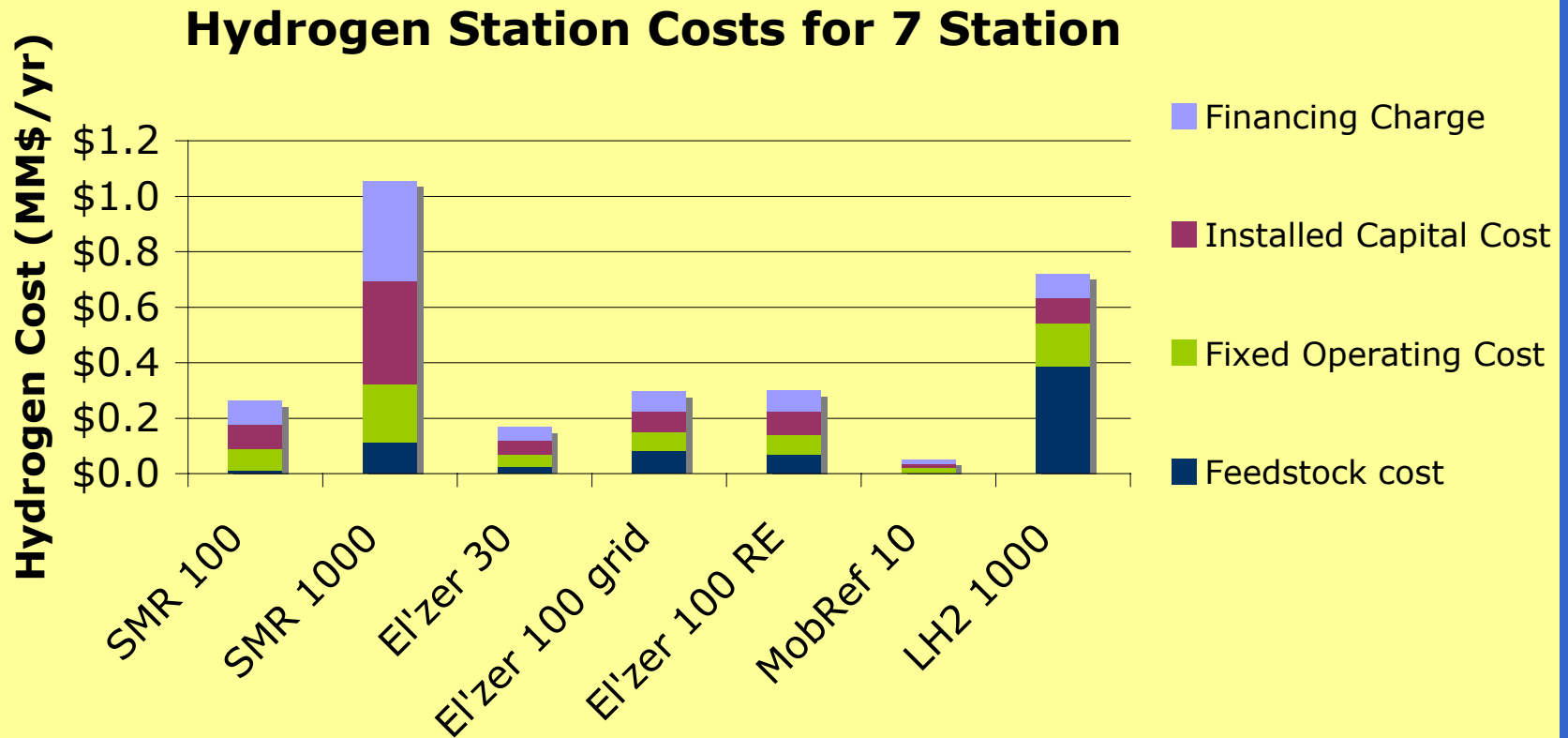
242 Stations to serve 5000 vehicles...

- Total Installed Capital Cost = **\$244 million**
 - Equipment Costs
 - Non-Capital Installation Costs
 - Permitting, Site prep, Engineering/Design, etc.
- Total Annual Cost = **\$52 million/yr**
 - Includes amortized capital cost (above) and annual operating cost
 - Feedstock, maintenance, rent, labor

Installed Station Capital Costs: 2010 Retail Scenario



Annual Station Costs: 2010 Retail Scenario



Scenarios for Success

- Scenario 1: Baseline
 - Retail hydrogen station (similar to commercial gasoline)
 - 2010 production volumes
- Scenario 2: Public Fleet Location
 - Higher throughput, capacity factor
 - Lower utility rates through incentives & industrial classification
- Scenario 3: Champion Applications
 - Leverage public-private partnerships, 0% financing
 - Higher production volumes
 - Strong local authority cooperation
 - Co-locate with DG app or industrial hydrogen user



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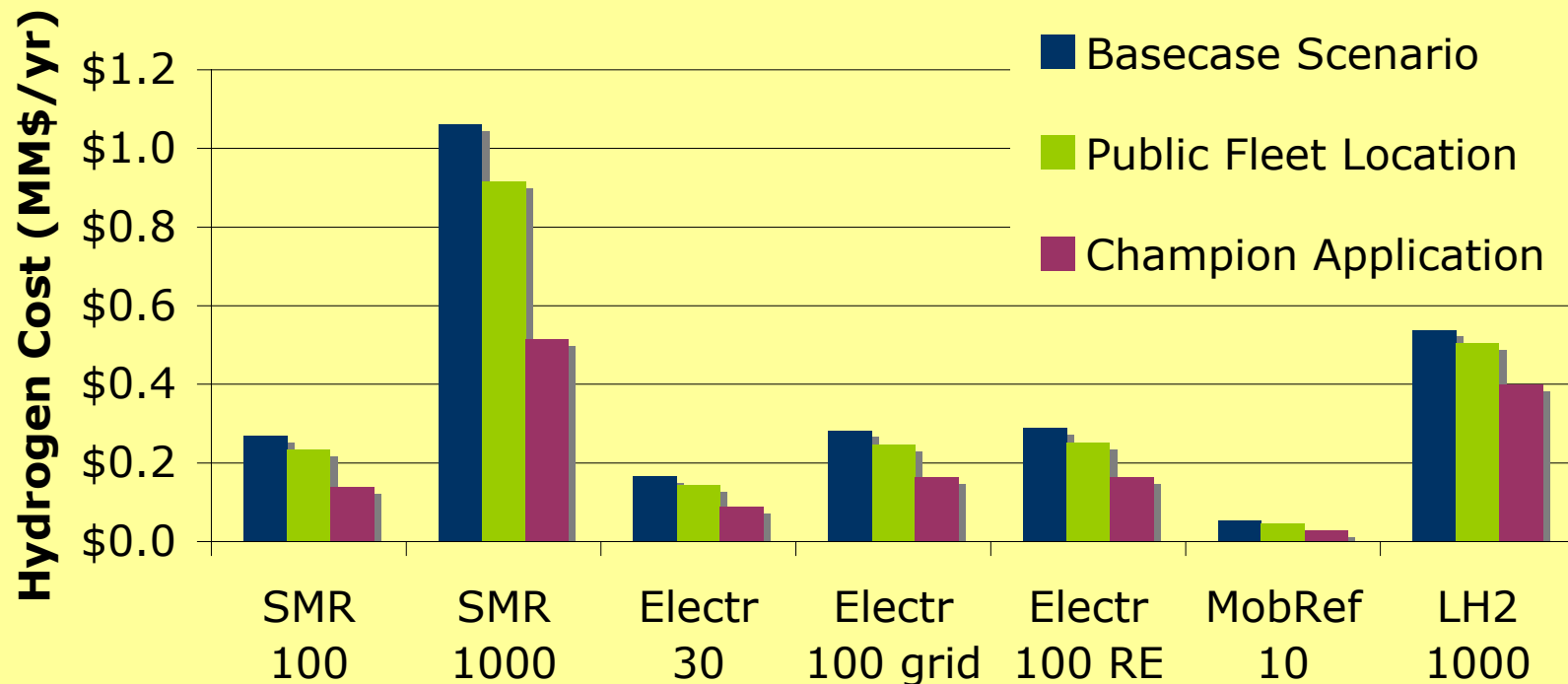
Assumptions Under 3 Scenarios

Assumption	Baseline Scenario	Public Fleet Location Scenario	Champion Application Scenario
Natural Gas (\$/MMBtu)	7	5	5
Electricity Cost (\$/kWh)	0.1	0.06	0.05
Capacity Factor	10%	10%	10%
Return on Investment (%)	10%	10%	0%
Production Volume Increase (from today)	2x	2x	5x
Real Estate Cost (\$/ft ² /month)	\$0.50	\$0.25	\$0
Installation Cost Reduction (%)	10%	20%	40%
% of Labor for Fuel Sale	50%	20%	0%
Contingency (%)	10%	10%	5%

Note: Capacity factor is held constant due to it's misleading effect on annual station cost. It should increase with Scenario 2 and 3.

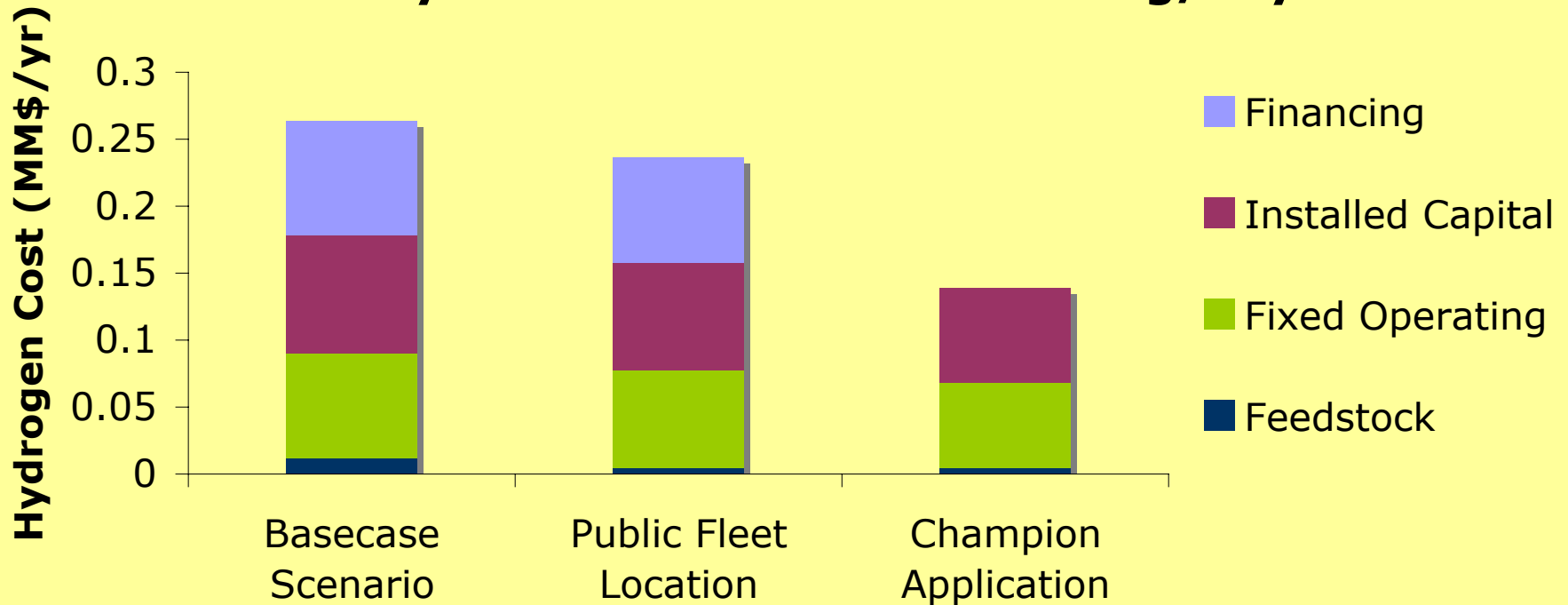
Scenarios for Success:

Scenario Analysis: Annual Station Costs for 7 Stations:

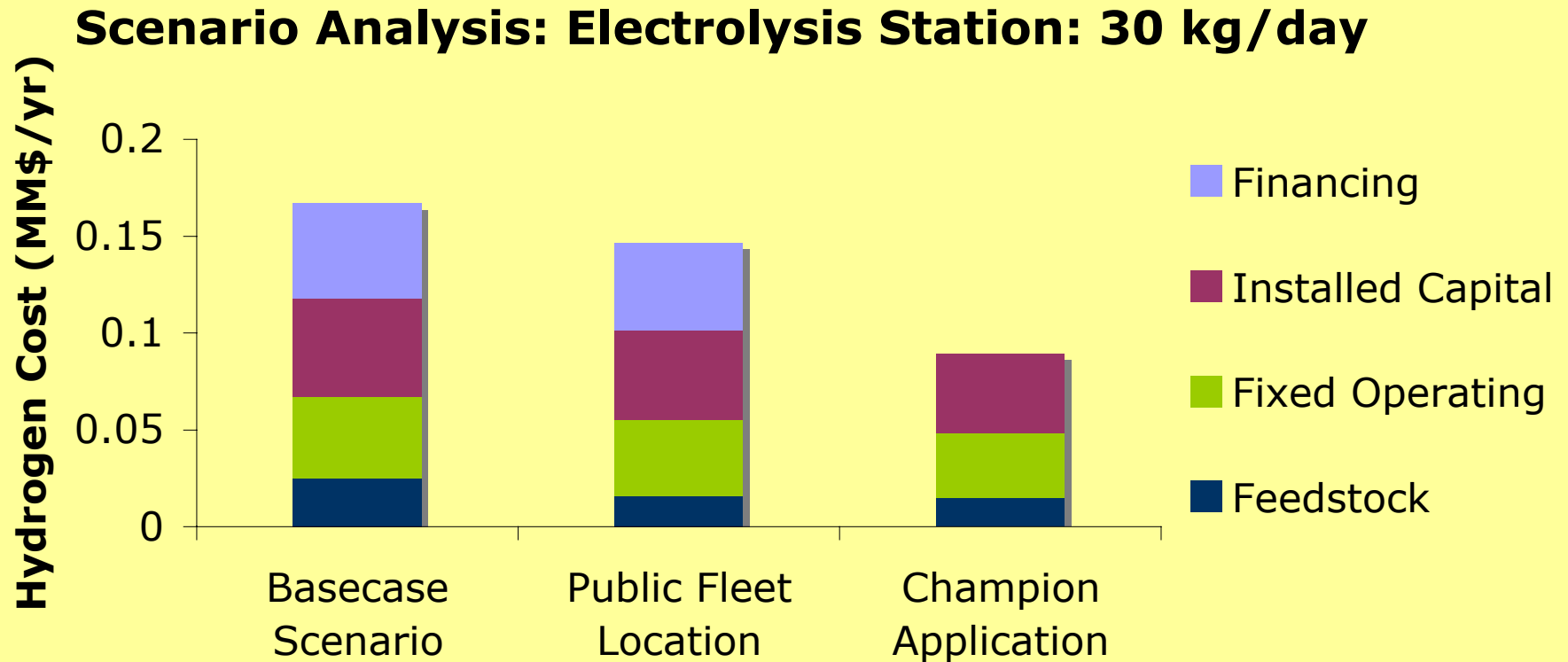


Scenarios for Success: Case 1

Scenario Analysis: Reformer Station: 100 kg/day

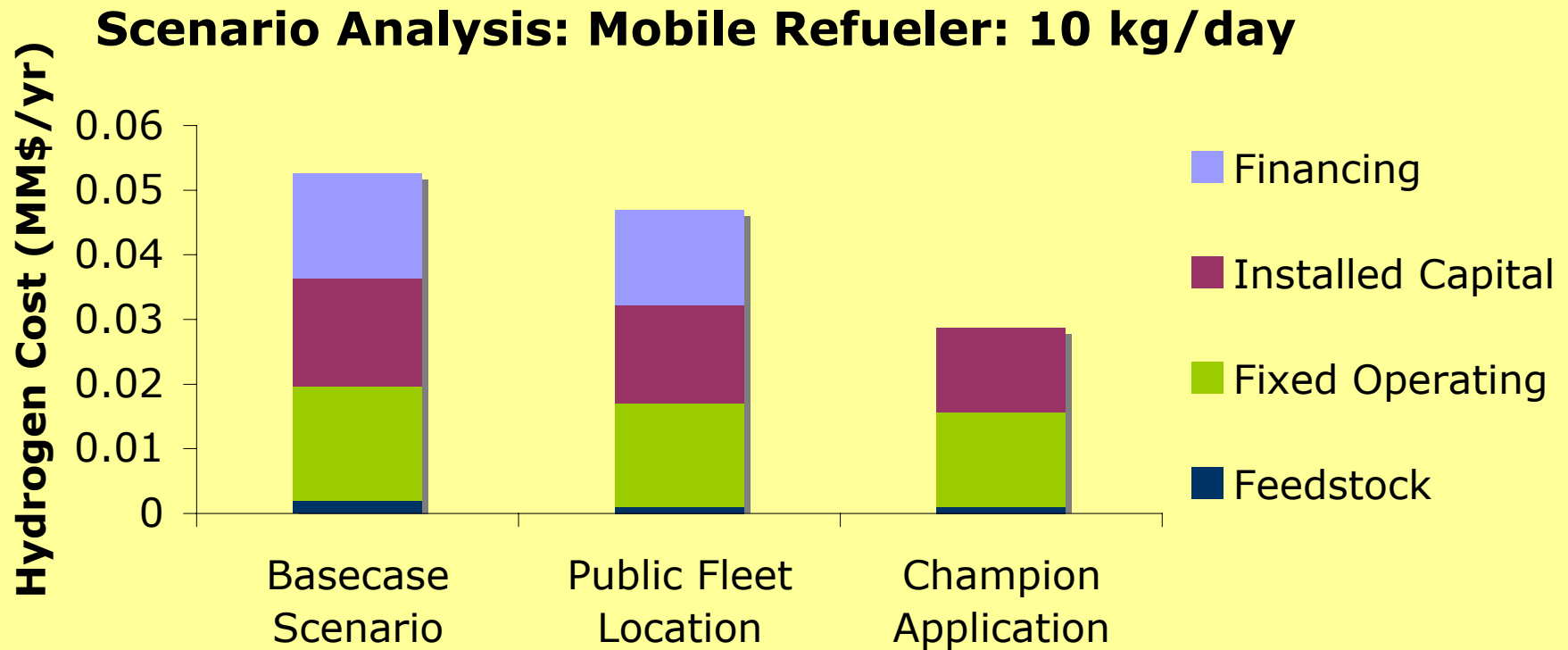


Scenarios for Success: Case 2



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Scenarios for Success: Case 3



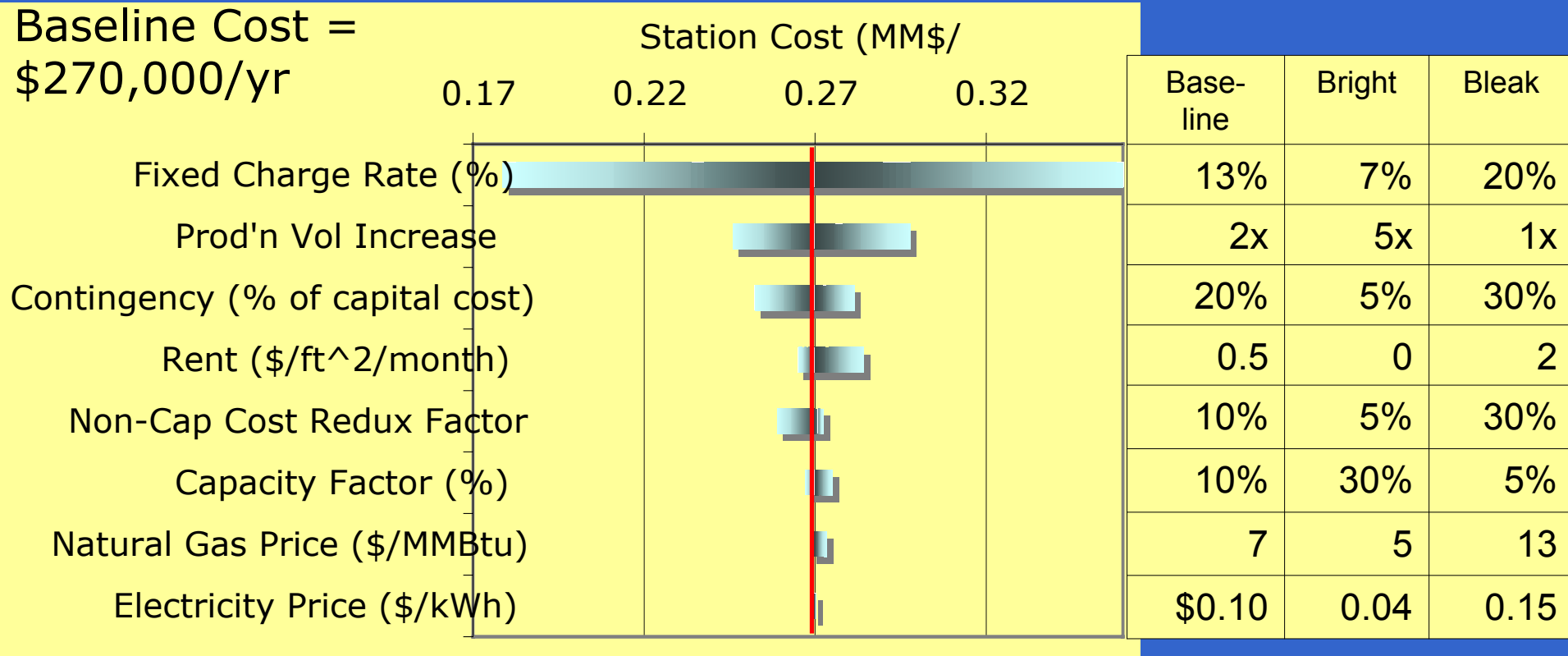
Sensitivity Analysis

	Basecase	Bright	Bleak
Natural Gas Price (\$/MMBtu)	7	5	10
Electricity Price (\$/kWh)	0.1	0.06	0.13
Capacity Factor (%)	70%	99%	40%
Fixed Charge Rate (%)	13%	7%	20%
Real Estate Cost (\$/ft^2/month)	1.5	1	2
Contingency (% of TIC)	10%	5%	15%
Prod'n Vol increase	Double	Current	quadruple
Non-Cap Cost Reduction Factor	10%	0.0%	20.0%



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Sensitivity Analysis: SMR 100



Note: Station cost rises with increasing capacity factor due to added operating costs.



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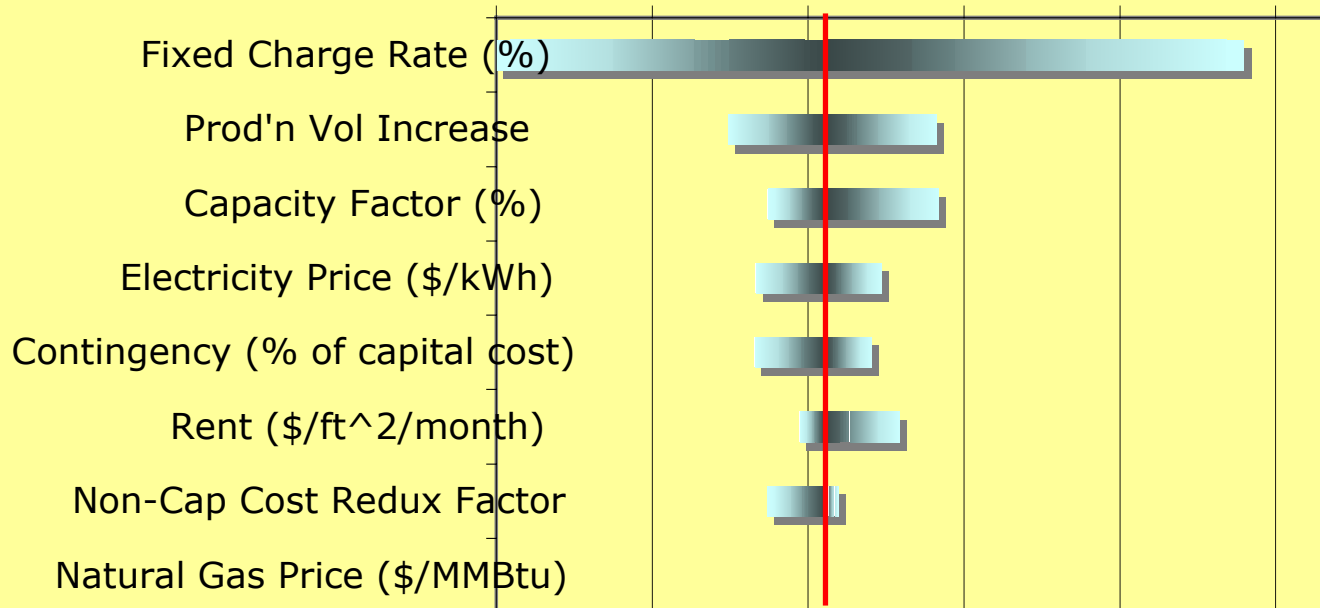
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Sensitivity Analysis: Electr'sis 100

Baseline Cost =
\$280,000/yr

Station Cost (MM\$,

0.22 0.25 0.28 0.31 0.34 0.37



Base-line	Bright	Bleak
13%	7%	20%
2x	5x	1x
10%	5%	30%
\$0.10	0.04	0.15
20%	5%	30%
0.5	0	2
10%	30%	5%
7	5	13

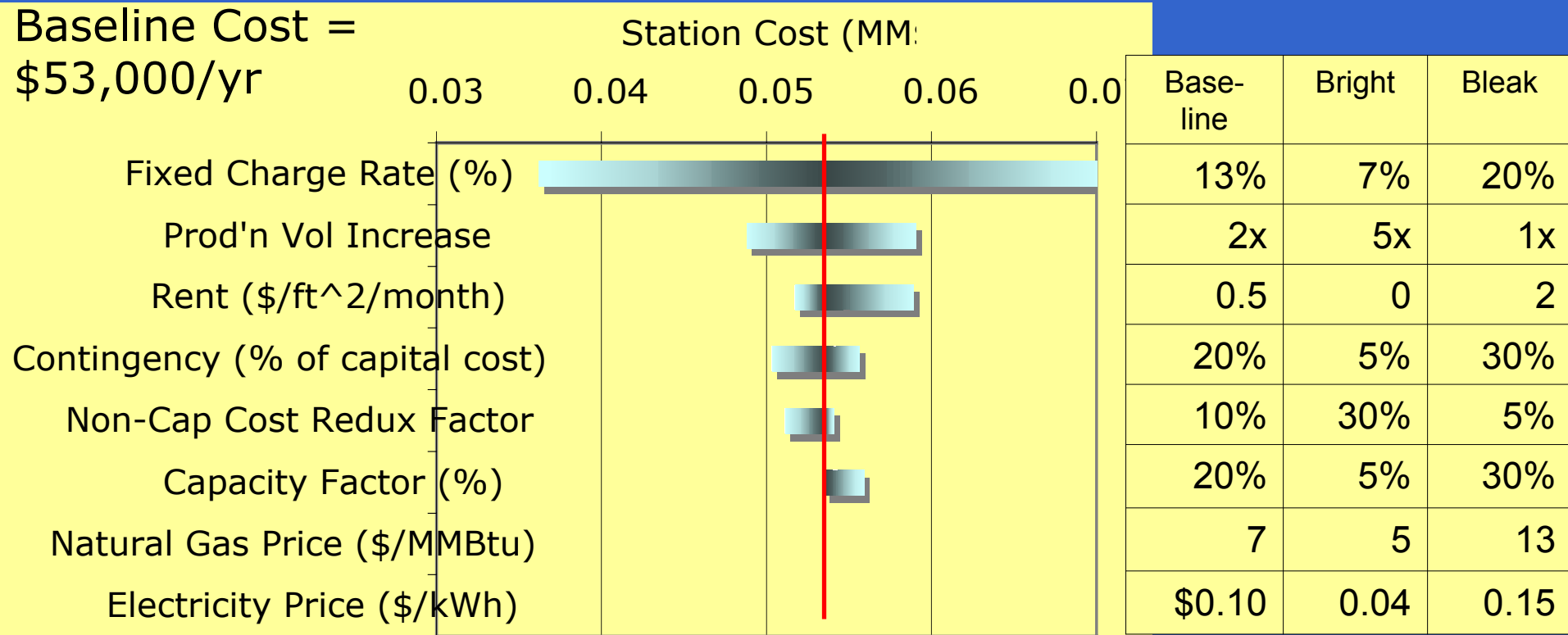
Note: Station cost rises with increasing capacity factor due to added operating costs.



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Sensitivity Analysis: MobRef 10



Note: Station cost rises with increasing capacity factor due to added operating costs.



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Conclusions

1. Choosing “Champion Applications” can reduce station cost up to ~50%
2. Station cost very sensitive to:
 - Production Volume increases
 - “0% Financing”
 - Contingency cost reduction
3. Low expected capacity factors in near term lead to lower annual station costs though higher hydrogen cost



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Acknowledgments

- UC Davis Institute of Transportation Studies
- Tiax, Stuart, Air Products, Chevron Texaco, Fuel Cell Energy, ISE Research, GM, Praxair, Proton Energy, Ztek, FTI, Shell, BOC, BP, Dynetech, H2Gen, Hydrogenics,
- REFERENCES:
Unnasch, S, Kassoy, E. and Powars, C (Feb, 2004), “Requirements for Combining Natural Gas and Hydrogen Fueling”, Consultant report for the California Energy Commission, Prepared by Tiax



$$\left[\frac{p^2}{2\mu} + V(r) \right] \psi(r) = E \psi(r)$$

Questions??



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